

This listing of claims will replace all prior versions, and listings, of claims in the application:

**Listing of Claims:**

1. Canceled
2. (Previously Presented) A process according to claim 31, in which Si/T of the modified zeolite is at least 20.
3. (Previously Presented) A process according to claim 31, in which Si/T of the modified zeolite is over 60.
4. (Previously Presented) A process according to claim 31, in which Si/T of the modified zeolite is at most 600.
5. (Previously Presented) A process according to claim 31, in which Si/T of the modified zeolite is at most 300.
6. (Previously Presented) A process according to claim 31, in which T is aluminum (Al).
7. (Previously Presented) A process according to claim 32, wherein the EU-1 zeolite is obtained by synthesis using at least one solution of an acid.
8. (Previously Presented) A process according to claim 31, wherein the zeolite is obtained using at least one heat treatment of ~~a EU-1 zeolite obtained by synthesis~~ the starting zeolite followed by at least one treatment with a solution of an acid.
9. (Previously Presented) A process according to claim 31, in which the EU-1 zeolite is obtained by dealuminating by at least one heat treatment followed by at least one treatment using a chemical dealuminating compound which is ammonium hexafluorosilicate, silicon tetrachloride, or ethylenediaminetetra-acetic acid, optionally in its sodium or disodium form.
10. (Previously Presented) A process according to claim 31, in which the EU-1 zeolite is obtained by dealuminating by at least one treatment with a

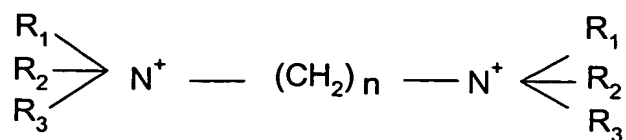
chemical dealuminating compound which is ammonium hexafluorosilicate, silicon tetrachloride, or ethylenediaminetetra-acetic acid, optionally in its sodium and disodium form.

11. Canceled
12. (Previously Presented) A process according to claim 31, wherein the zeolite catalyst comprises at least one matrix and 0.5% to 99.5% by weight of EU-1 zeolite with respect to the matrix + zeolite mixture.
13. Canceled
14. Canceled
15. Canceled
16. Canceled
17. (Previously Presented) A process according to claim 31, in which the hydro-dehydrogenating element is niobium and/or rhenium.
18. Canceled
19. (Previously Presented) A process for improving the pour point of a feed comprising paraffins containing more than 10 carbon atoms, in which process the feed to be treated is brought into contact with a catalyst based on EU-1 zeolite, at least partially in its acid form, and at least one hydro-dehydrogenating element, at a temperature of 170°C to 500°C, a pressure of 1 to 250 bar and at an hourly space velocity of 0.05 to 100 h<sup>-1</sup>, the presence of hydrogen in a proportion of 50 to 2000 l/l of feed.
20. (Previously Presented) A process according to claim 19, in which the hydro-dehydrogenating element is a noble group VIII element.
21. (Previously Presented) A process according to claim 19, in which the hydro-dehydrogenating element is a combination of at least one group IV metal or compound and at least one non noble group VIII metal or compound.
22. (Previously Presented) A process according to claim 21, in which the catalyst contains phosphorous.
23. (Previously Presented) A process according to claim 19, in which the catalyst contains a matrix and 0.5% to 99.9% by weight of EU-1 zeolite with respect to the matrix +

zeolite mixture.

24. Canceled
25. (Previously Presented) A process according to claim 19, in which the initial boiling point of the feed is over 175°C.
26. (Previously Presented) A process according to claim 19, in which the initial boiling point of the feed is over 280°C.
27. (Previously Presented) A process according to claim 19, in which the initial boiling point of the feed is over 380°C.
28. (Previously Presented) A process according to claim 19, in which the feed comprises paraffins containing 15 to 50 carbon atoms.
29. (Previously Presented) A process according to claim 19, in which the feed contains paraffins containing 15 to 40 carbon atoms.
30. (Previously Presented) A process according to claim 19, in which the feed to be treated is a hydrocarbon feed selected from the group consisting of middle distillates, gas oils, vacuum residues, hydrocracking residues, paraffins from the Fischer-Tropsch process, synthesized oils, gas oil cuts and FCC middle distillates, oils, and polyalphaolefins.
31. (Previously Presented) A process for improving the pour point of a feed comprising paraffins containing more than 10 carbon atoms, comprising contacting the feed with a catalyst based on EU-1 zeolite, at least partially in its acid form, and at least one hydro-dehydrogenating element, wherein the EU-1 zeolite comprises silicon and an element T which is Al, Fe, Ga, or B, produced by a process in which at least a portion of elements T are removed from a starting zeolite, whereby the modified zeolite has a global atomic ratio Si/T higher than that of the starting zeolite, by at least 10% of the Si/T ratio of the starting zeolite.
32. (Currently Amended) A process for improving the pour point of a feed comprising paraffins containing more than 10 carbon atoms, in which process the feed to be treated is brought into contact with a catalyst based on EU-1 zeolite, at least partially in its acid form, and at least one hydro-dehydrogenating element, at a temperature of 170°C to 500°C, a pressure of 1 to 250 bar and at an hourly space velocity of 0.05 to 100 h<sup>-1</sup>, the presence of hydrogen in a proportion of 50 to 2000 l/l of feed and wherein the EU-1 zeolite is produced with

at least one alkylated derivative of a polymethylene  $\alpha$ - $\omega$  - diamine having the formula

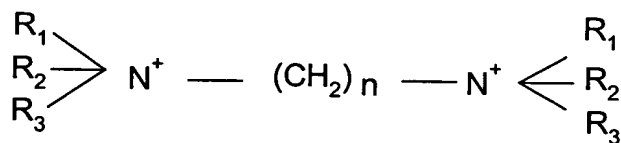


or an amine degradation product thereon, wherein n is 3 to 12 and R<sub>1</sub> to R<sub>6</sub> are each independently alkyl or hydroxyalkyl groups, containing from 1 to 8 carbon atoms and up to five of the groups R<sub>1</sub>-R<sub>6</sub> can be hydrogen.

33. (Previously Presented) A process according to claim 32, wherein the polymethylene  $\alpha$ - $\omega$  diamine is an alkylated hexamethylene diamine.

34. (Previously Presented) A process according to claim 33, wherein the polymethylene  $\alpha$ - $\omega$  diamine is hexamethonium salt.

35. (Currently Amended) A process for improving the pour point of a feed comprising paraffins containing more than 10 carbon atoms, in which process the feed to be treated is brought into contact with a catalyst based on EU-1 zeolite, at least partially in its acid form, and at least one hydro-dehydrogenating element, wherein the EU-1 zeolite comprises silicon and an element T which is Al, Fe, Ga, or B, produced by a process in which at least a portion of elements T are removed from a starting zeolite, whereby the modified zeolite has a global atomic ratio Si/T higher than that of the starting zeolite, by at least 10% of the Si/T ratio of the starting zeolite and wherein the EU-1 zeolite is produced with at least one alkylated derivative of a polymethylene  $\alpha$ - $\omega$  - diamine having the formula



of an amine degradation product thereon, wherein n is 3 to 12 and R<sub>1</sub> to R<sub>6</sub> are each independently alkyl or hydroxyalkyl groups, containing from 1 to 8 carbon

atoms and up to five of the groups  $R_1$ - $R_6$  can be hydrogen.

36. (Previously Presented) A process according to claim 35, wherein the polymethylene  $\alpha$ - $\omega$  diamine is an alkylated hexamethylene diamine.

37. (Previously Presented) A process according to claim 36, wherein the polymethylene  $\alpha$ - $\omega$  diamine is hexamethonium salt.